

Polyoxometalate-derived N@Mo₂C/V₂O₃ cluster heterostructure for accelerated alkaline hydrogen evolution reaction

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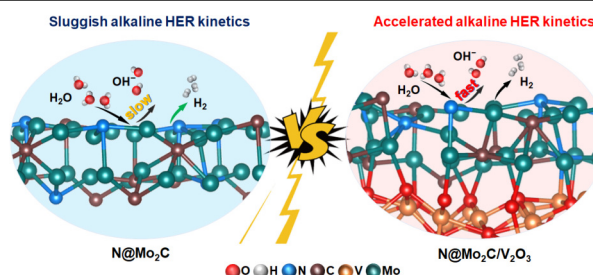


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ABSTRACT: The hydrogen evolution reaction (HER) in alkaline water electrolysis is fundamentally limited by the high energy barrier associated with water dissociation. Herein, we report the development of self-supported nitrogen-doped molybdenum carbide and vanadium oxide cluster heterostructures (N@Mo₂C/V₂O₃) on carbon fiber paper using organoimido-derivatized molybdovanadate nanoclusters as precursors. Experimental results and theoretical calculations demonstrate that the engineered cluster heterointerfaces significantly reduce the energy barrier of the rate-determining step, accelerating HER kinetics. Moreover, V₂O₃ acts as a cocatalyst that enhances hydrophilicity of the N@Mo₂C/V₂O₃ and, versus pristine N@Mo₂C, facilitates hydrogen desorption from the composite. The optimized N@Mo₂C/V₂O₃ cluster heterostructure exhibits exceptional electrocatalytic performance, delivering a current density of 300 mA·cm⁻² at an overpotential of merely 191 mV and maintaining stability over 400 h of continuous operation. When integrated into an alkaline water electrolyzer, the system requires only 1.94 V to achieve an industrially relevant current density of 500 mA·cm⁻², outperforming commercial platinum–carbon catalysts. These findings offer new perspectives and valuable insights into the development of efficient, stable, and economical noble metal-free electrocatalysts for green hydrogen production.



KEYWORDS: polyoxometalates, clusters, heterostructures, electrocatalysis, hydrogen evolution reaction

1 Introduction

Hydrogen production via water electrolysis, as a clean and sustainable energy-generation technology, holds profound significance in addressing the global energy crisis and alleviating environmental pollution [1]. By integrating electrolysis with renewable energy sources, abundant water resources can be effectively transformed into high-value hydrogen energy, thus providing steadfast support and a robust foundation for energy transition and eco-friendly green development [2, 3]. Compared with acidic water electrolysis, alkaline water electrolysis demonstrates distinct advantages, including lower cost, greater technological maturity, and superior electrode durability. However, despite these merits, the efficiency of hydrogen production in

alkaline environments is significantly hindered by inherent complexity and sluggish kinetics associated with water adsorption and dissociation as well as the adsorption and desorption of reaction intermediate during the hydrogen evolution reaction (HER). These kinetic limitations not only reduce overall hydrogen production efficiency but also lead to substantial energy losses, presenting considerable challenges for practical applications [4]. Furthermore, under industrial operating conditions, namely high temperature (~ 80 °C), highly alkaline electrolyte (~ 30 wt.% KOH), and high current densities (> 300 mA·cm⁻²), extensive gas bubbling is generated during alkaline water electrolysis to enhance hydrogen production efficiency. This vigorous gas evolution continuously strips the catalyst surface, which places strict requirements on the stability of the electrode [5, 6]. These harsh conditions impose stringent requirements on electrode durability, prompting the development of self-supported catalysts that directly integrate active components into the electrode structure. Such designs not only enhance mechanical stability but also reduce manufacturing costs compared with conventional powder-based catalyst systems [7–10]. Moreover, the transition from laboratory-scale three-electrode configurations to industrial alkaline water electrolyzers presents

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substantial challenges, particularly for powder catalysts that rely on polymeric binders. This well-defined aqueous electrolyte environment of a three-electrode cell fails to replicate the harsh conditions of zero-gap alkaline electrolyzers, which operates at elevated temperatures, high current densities, and under intense gas evolution. Consequently, the polymeric binders used to immobilize powder catalysts are prone to degradation, leading to catalyst detachment and rapid deactivation under these industrial operating conditions [6]. Consequently, there is an urgent need to develop integrated HER electrodes that combine high catalytic activity with long-term stability for practical industrial applications [11, 12].

The development of cost-effective electrocatalysts based on earth-abundant elements has become critically important owing to the high cost and limited availability of noble-metal, platinum-based materials [13]. Among the alternative candidates, molybdenum carbides (MoC and Mo₂C) have emerged as particularly promising HER catalysts, owing to their platinum-like electronic properties, high electrical conductivity, and exceptional electrochemical stability [14–16]. However, despite their advantages, pristine Mo₂C binds hydrogen quite strongly because of the high density of the empty Mo d orbitals, which hinders the desorption of active hydrogen [17]. Tuning the electronic structure of Mo₂C through heteroatom incorporation can effectively improve its hydrogen adsorption energy and enhance HER catalytic performance [18–20]. Nevertheless, in alkaline media, HER kinetics involve additional critical steps beyond hydrogen adsorption, including water molecule adsorption and activation as well as hydroxyl intermediate (OH[−]) desorption, which together can govern the overall reaction rate [21–23]. Single-component catalysts typically fail to simultaneously satisfy all these kinetic requirements, often resulting in suboptimal catalytic performance [24]. Therefore, the integration of two or more catalytic materials to form heterostructures has emerged as a highly effective strategy for boosting catalyst activity.

Recent studies have demonstrated that the high electronegativity of V₂O₃ can effectively destabilize surface-adsorbed water molecules, thereby enhancing water polarization and significantly accelerating water dissociation kinetics [25, 26]. Moreover, V₂O₃ exhibits extremely weak hydrogen binding energy [25], which can promote efficient hydrogen desorption at heterointerfaces. In this context, constructing heteroatom-doped Mo₂C/V₂O₃ heterojunctions in self-supported architectures may provide an effective strategy to overcome kinetic limitations in alkaline HER systems. Polyoxometalates (POMs), a class of anionic clusters comprising early transition metals (Mo, V, and W) and oxygen [27], offer unique advantages for catalyst design [28–30], including atomic-level structural precision and uniform sizes (~ 1 nm) [31–37]. In particular, POMs are well suited as precursors for constructing molybdenum carbide-based heterojunctions [19, 38]. POMs enable not only the targeted incorporation of heteroatoms through organic functionalization but also the precise engineering of POM frameworks containing specific metallic heteroatoms, making them exceptionally versatile building blocks for advanced catalyst development [15, 18, 39, 40].

Heterostructured catalysts, including metal–carbide [41], carbide–oxide [42], nitride–carbide [43, 44], nitride–oxide [26, 45] systems, among others [46], have emerged as powerful platforms for tuning interfacial electronic structures. Lattice mismatch and work-function differences across heterointerfaces create built-in electric fields and charge redistribution regions [24], which

modulate the adsorption energies of key intermediates and accelerate electron transfer. Particularly, oxide–nitride heterostructures integrate the strong water activation capability of oxides with the high conductivity and favorable hydrogen adsorption of carbides [26], thereby enabling balanced Volmer–Heyrovsky kinetics in the alkaline HER [45]. Consequently, the rational design of such electronically coupled heterointerfaces represents an effective strategy to overcoming the intrinsic limitations of single-phase catalysts and achieving superior catalytic efficiency.

Inspired by these studies, we synthesized a Mo–V POM precursor consisting of a polyarylimido-stabilized molybdovanadate cluster ([V₄Mo₃O₁₄(NAr)₃(l2-NAr)₃]^{3−}), denoted as Mo3V4-NAr [33]. Subsequent one-step pyrolysis of this precursor yielded N@Mo₂C/V₂O₃ cluster heterostructures featuring abundant heterogeneous interfaces.

This innovative approach successfully addresses two fundamental challenges in heterostructure fabrication: precise control over interfacial formation and the limited interfacial contact areas typically observed in conventional systems. By leveraging the well-defined molecular architecture of the Mo3V4-NAr POM precursors stabilized by arylimido ligands, nanocrystal growth was effectively confined during pyrolysis, resulting in the formation of uniform N@Mo₂C/V₂O₃ cluster heterostructures. The resulting heterostructured architecture not only effectively enhances surface hydrophilicity and accelerates reaction kinetics but also optimally modulates the electronic structure and interfacial charge distribution of the N@Mo₂C/V₂O₃ cluster heterostructure. These synergistic effects can effectively reduce the energy barrier of the rate-determining step and optimize the binding energies of key HER intermediates (OH[−] and H[•]). Consequently, the optimized N@Mo₂C/V₂O₃ cluster heterostructure exhibits remarkable catalytic activity and robust high-current stability under alkaline conditions for the HER, achieving a current density of 300 mA·cm^{−2} at an overpotential of just 191 mV and maintaining stable operation for over 400 h, significantly outperforming conventional 20 wt.% Pt/C catalysts. Moreover, when implemented in an alkaline water electrolyzer (AWE), this catalyst requires only 1.94 V to drive a current density of 500 mA·cm^{−2}, demonstrating its immense potential for practical and industrial applications.

2 Method

2.1 Preparation of N@Mo₂C/V₂O₃

Carbon fiber paper (CFP) was first subjected to ultrasonic cleaning in deionized water, ethanol, and acetone, followed by drying in an oven. The Mo3V4-6NAr POM precursor was subsequently redissolved in acetonitrile and homogenized via ultrasonication to obtain a homogeneous solution. This solution was drop-cast onto the precleaned CFP to ensure complete infiltration. After drying, the CFP was uniformly coated with *in situ*-grown POMs. Subsequently, the coated CFP was transferred to a tubular furnace for thermal treatment at 650 °C for 3 h under a reducing atmosphere (8% H₂/Ar), yielding the N@Mo₂C/V₂O₃ cluster heterostructure. To investigate the influence of calcination temperature on phase composition and alkaline HER electrocatalytic performance, additional comparative samples were synthesized using identical procedures at varying temperatures (600, 700, 800, and 900 °C).

2.2 Preparation of N@Mo₂C and V₂O₃

For comparison, N@Mo₂C and V₂O₃ catalysts were synthesized separately using [(C₄H₉)₄N]₂[Mo₆O₁₃(NC₆H₅)₆] (denoted as Mo6-6NAr) and [(C₄H₉)₄N]₃[H₃V₁₀O₂₈] (abbreviated as V10) as precursors, respectively. Except for the use of different precursors, all synthesis procedures were identical to those used for the N@Mo₂C/V₂O₃ composite, ensuring consistency across all prepared samples.

2.3 Electrochemical measurements

The HER performance of commercial 20 wt.% Pt/C, N@Mo₂C/V₂O₃, N@Mo₂C, and V₂O₃ catalysts was evaluated

using a standard three-electrode system at room temperature with a CHI760E electrochemical workstation. For the Pt/C benchmark catalyst, a homogeneous catalyst ink was prepared by dispersing 5.0 mg of 20 wt.% Pt/C in 950 μ L of a water/isopropanol mixture (1:1 v/v), followed by the addition of 50 μ L of 5 wt.% Nafion solution. The resulting mixture was ultrasonicated for 30 min to ensure uniform dispersion. Subsequently, 100 μ L of the catalyst ink was drop-cast onto a 1 cm $\times$ 1 cm carbon paper substrate. After drying, the working electrode was obtained with a Pt/C loading of 0.5 mg $\cdot$ cm⁻². A carbon rod and a reversible hydrogen electrode (RHE) were used as the counter and reference electrodes, respectively. Linear sweep voltammetry was performed over a potential window of -0.5 to 0.05 V (vs. RHE) at a scan rate of 5 mV $\cdot$ s⁻¹, with 95% *i*R compensation applied. Tafel slopes were determined by linear fitting of the corresponding polarization curves. The electrochemical double-layer capacitance (*C*_{dl}) was determined from cyclic voltammetry (CV) measurements conducted in a non-Faradaic potential range (0.1–0.3 V vs. RHE) at varying scan rates (10–60 mV $\cdot$ s⁻¹). Additionally, electrochemical impedance spectroscopy (EIS) was performed at open-circuit potential over a frequency range of 0.01–100,000 Hz.

2.4 Solar-driven water electrolysis cell testing

The system was constructed by connecting commercial solar panels

(12 V, 12 W output under standard illumination) to a two-electrode setup. Hydrogen gas produced by the integrated system under natural sunlight irradiation was collected using the water displacement method.

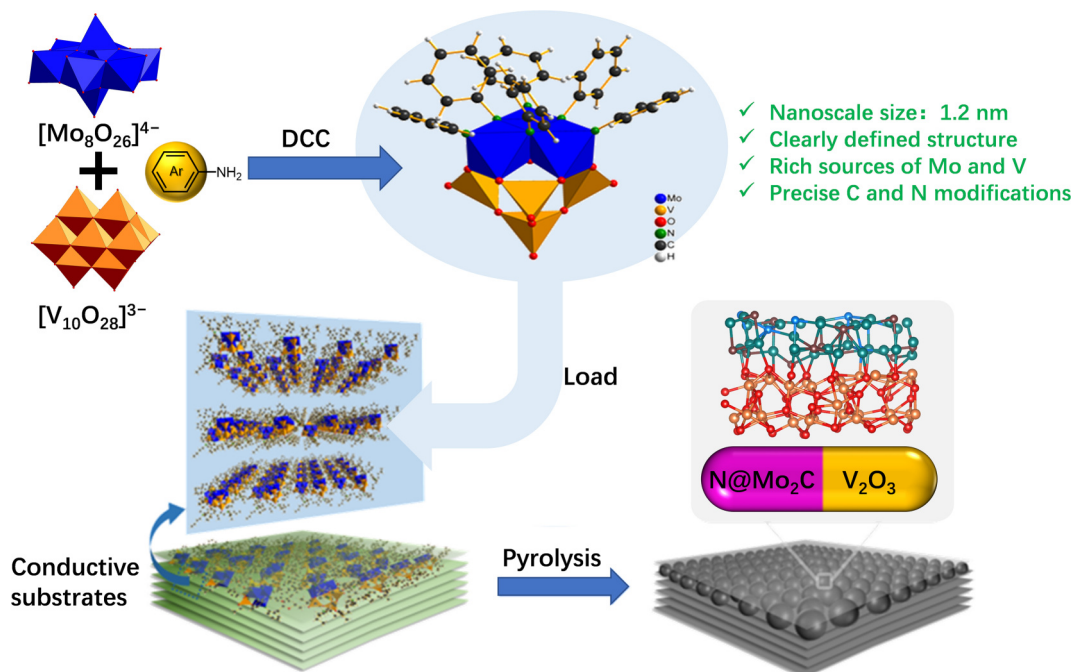
2.5 Alkaline water electrolyzer testing

An AWE was configured in a two-electrode setup for evaluating the electrolysis efficiency of the catalysts. The cathode was a self-supporting N@Mo₂C/V₂O₃ electrode with a large geometric area of 12.56 cm² (radius = 2 cm), along with a commercial Zirfon separator. The anode consisted of either commercial Raney nickel (purchased from Anhui Weishui New Energy Technology Co., Ltd.) or a NiFe layered double hydroxide (NiFe-LDH) catalyst [47] for comparative assessment. The electrolyte was a 30% KOH solution, and all electrochemical measurements were performed at 60 $^{\circ}$ C under atmospheric pressure. Polarization curves were recorded from open-circuit voltage to high current densities, while galvanostatic stability tests were conducted at a constant current density of 500 mA $\cdot$ cm⁻² to evaluate long-term stability of the as-prepared catalysts. All assembly tests were repeated three times, and the results were averaged for accuracy. To further assess the performance of the AWE, additional tests were conducted at varying temperatures (20, 40, and 60 $^{\circ}$ C).

3 Results and discussion

3.1 Synthesis of electrocatalysts

The synthetic route for the N@Mo₂C/V₂O₃ cluster heterostructure is schematically illustrated in Scheme 1, with detailed procedures provided in the Methods section. Initially, a well-defined Mo₃V₄-6NAr POM precursor was synthesized (Fig. S1 in the Electronic Supplementary Material (ESM)), comprising six arylimido ligands covalently functionalized on the organometallic POM framework. This precisely engineered precursor features an atomic Mo:V ratio of 3:4 within each molecule. Concurrently, the strategic



Scheme 1 Schematic illustration of the synthesis of N@Mo₂C/V₂O₃.

incorporation of Mo–N bonds via the arylimido ligands enables controllable nitrogen doping into Mo_2C [15], allowing for atomic-level nitrogen doping in Mo_2C .

3.2 Morphological and structural characterizations

The scanning electron microscopy (SEM) image in Fig. S2(a) in the ESM displays the morphology of the pristine CFPs, with individual carbon fibers exhibiting a diameter of $\sim 8\ \mu\text{m}$. The fiber surfaces exhibit a rough texture with distinct longitudinal striations, which can facilitate the heterogeneous nucleation and recrystallization of POM molecules. Figures S2(b)–S2(d) in the ESM illustrate the morphologies of Mo3V4-6NAr, Mo6-6NAr, and V10 grown on the carbon fibers. SEM images clearly demonstrate that the POM molecules form a homogeneous conformal coating on the fiber surfaces, completely encapsulating the substrates. This uniform coating ensures robust interfacial adhesion between the POM molecules with the conductive carbon paper during subsequent thermal processing. The POM-loaded carbon paper was subsequently pyrolyzed, and the resulting products were subjected to comprehensive phase composition analysis and microstructural characterization. The X-ray diffraction (XRD) patterns shown in Fig. 1(a) demonstrates that the pyrolysis product of Mo6-6NAr exhibits diffraction peaks consistent with the standard reference

pattern PDF#72-1683 for molybdenum carbide (Mo_2C). This confirms the successful formation of phase-pure Mo_2C through pyrolysis. By contrast, the V10-derived product exclusively matches the vanadium(III) oxide reference (PDF#71-0343), verifying the formation of V_2O_3 . The XRD pattern of the Mo3V4-6NAr pyrolysis product exhibits well-defined diffraction peaks corresponding to both Mo_2C and vanadium oxide (V_2O_3), unambiguously demonstrating the formation of a $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure. Notably, the diffraction peaks of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ are broader than those of the individual $\text{N@Mo}_2\text{C}$ and V_2O_3 . This peak broadening suggests mutual inhibition of crystalline growth between these two heterostructured components (Fig. S3 and Table S2 in the ESM), effectively suppressing nanoparticle aggregation and Ostwald ripening [32, 48].

As shown in Fig. S3 in the ESM, $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$, $\text{N@Mo}_2\text{C}$, and V_2O_3 were uniformly deposited on carbon fibers, forming a robust catalyst layer strongly adhered to the carbon paper substrate. This intimate contact facilitates efficient electron transfer between the active materials and the conductive carbon paper. High-magnification imaging (Fig. 1(b) and Fig. S3(d) in the ESM) revealed that the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ surface consists of abundant nanosheets with pronounced protrusions. By contrast, $\text{N@Mo}_2\text{C}$ exhibits a smoother morphology with densely packed nanoparticle

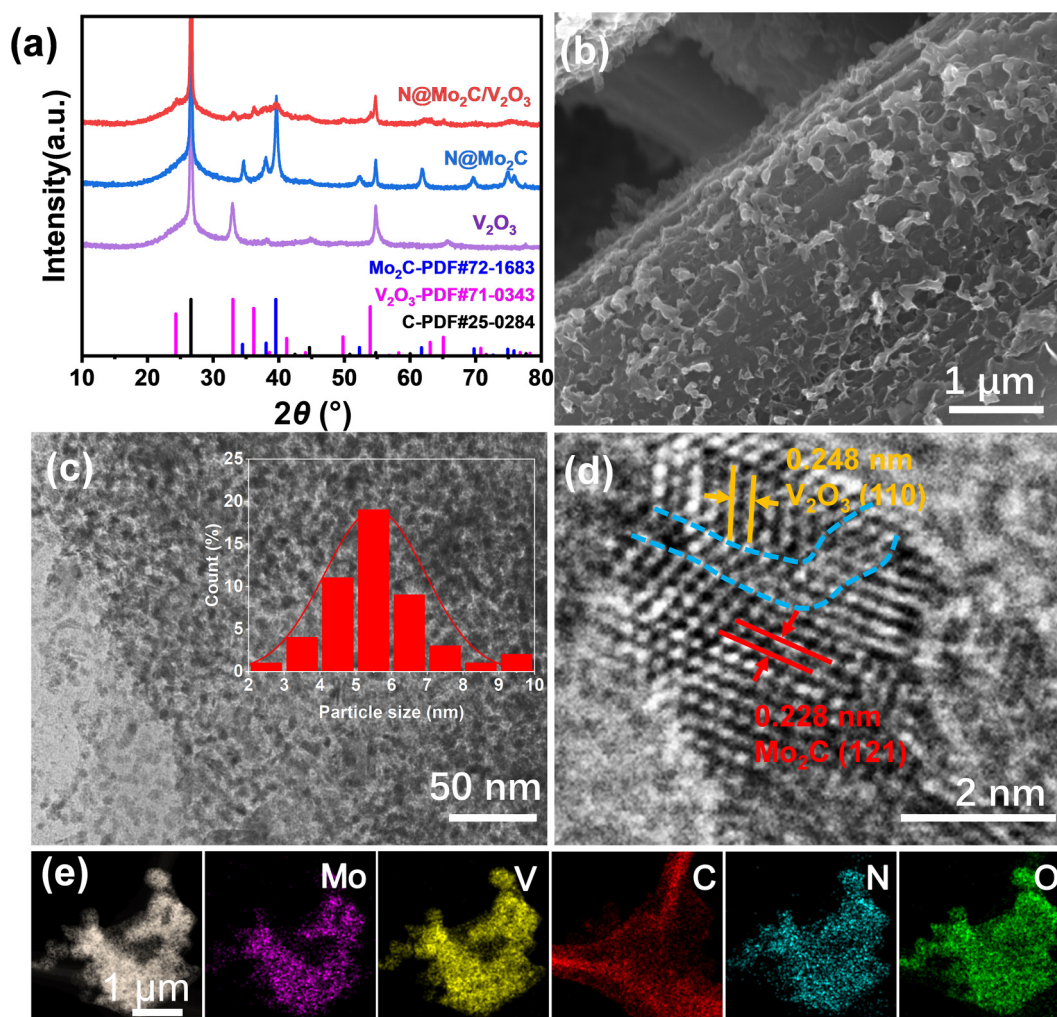


Figure 1 (a) XRD patterns of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$, $\text{N@Mo}_2\text{C}$, and V_2O_3 . (b) SEM image of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$. (c) TEM image and nanoparticle size distribution histogram (insert) of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$. (d) HRTEM image of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$. The blue dashed line(s) in the figure represent the heterointerface between $\text{N@Mo}_2\text{C}$ and V_2O_3 . (e) EDX elemental mappings of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$.

(Fig. S3(e) in the ESM), whereas V_2O_3 displays larger, well-defined nanosheets with a porous structure (Fig. S3(f) in the ESM). Notably, the nanosheets in $N@Mo_2C/V_2O_3$ are significantly finer than those observed in pristine V_2O_3 . Moreover, transmission electron microscopy (TEM) reveals distinct structural differences among the catalysts. The V_2O_3 catalyst consists of nanoparticles with diameters of 20–30 nm (Fig. S3(i) in the ESM), whereas the $N@Mo_2C$ catalyst consists of smaller nanoparticles (~ 10 nm, Fig. S3(h) in the ESM). By contrast, the $N@Mo_2C/V_2O_3$ cluster heterostructure exhibits a highly dispersed nanosheet morphology with ultrafine nanoparticles of only 5–6 nm (Fig. 1(c) and Fig. S3(g) in the ESM). These observations suggest that the existence of V_2O_3 modifies the structural evolution of $N@Mo_2C$ on the carbon paper substrate, resulting in a heterojunction catalyst with significantly reduced particle size and an open, porous architecture. The catalysts were further characterized for their specific surface area and pore structure using the Brunauer–Emmett–Teller (BET) and Barrett–Joyner–Hallender methods [33, 49], respectively. The $N@Mo_2C/V_2O_3$ cluster heterostructure exhibited a high BET surface area of $79.326 \text{ m}^2\text{g}^{-1}$ with an average pore size of 3.43 nm (Fig. S4 in the ESM). Raman spectroscopy (Fig. S5 in the ESM) suggests that the incorporated amorphous carbon likely inhibits $N@Mo_2C/V_2O_3$ nanoparticle growth while stabilizing the nanosheet morphology of $N@Mo_2C/V_2O_3$ [15].

Furthermore, a representative high-resolution TEM (HRTEM) image is shown in Fig. 1(d), clearly revealing well-defined lattice fringes with interplanar spacings of 0.228 and 0.248 nm, which correspond to the (121) plane of Mo_2C and the (110) plane of V_2O_3 , respectively. A distinct heterojunction interface forms between these two crystallographic planes, as marked by the blue dashed line in Fig. 1(d). Energy-dispersive X-ray spectroscopy (EDX) elemental mapping further demonstrates the uniform distribution of Mo, V, C, N, and O throughout the $N@Mo_2C/V_2O_3$ composite, with no observable agglomeration (Fig. 1(e)). By combining EDX data with the inductively coupled plasma atomic emission spectrometry results (Table S1 in the ESM), the atomic mass fractions of Mo, V, and N in $N@Mo_2C/V_2O_3$ were determined to be 17.07%, 10.31%, and 6.24%, respectively. Interestingly, the derived atomic ratios of Mo:V (1:1.14) and Mo:N (1:2.42) closely match those of the initial Mo_3V_4-6NAr precursor (Mo:V = 1:1.33, Mo:N = 1:2), indicating that the Mo, V, and N heteroatoms in the POM molecular precursor are well retained in the final catalyst, ultimately forming a cluster heterojunction. For the $N@Mo_2C/V_2O_3$ cluster heterostructure, the carbon content was excluded from the quantitative analysis owing to its excessive contribution from the carbon fiber substrate following ultrasonic detachment and mechanical grinding.

To elucidate the chemical composition and valence states of the $N@Mo_2C/V_2O_3$ cluster heterostructure, X-ray photoelectron spectroscopy (XPS) was employed. As shown in Fig. 2(a), the XPS survey spectrum confirms the presence of Mo, V, C, N, and O as the primary elements of the $N@Mo_2C/V_2O_3$ cluster heterostructure. The high-resolution Mo 3d spectrum (Fig. 2(b)) reveals three distinct doublets corresponding to different molybdenum oxidation states. The binding energies observed at 228.5 and 231.5 eV are assigned to the $3d_{5/2}$ and $3d_{3/2}$ orbitals of Mo^{3+} in Mo_2C [8, 15], respectively. Peaks at 229.4 and 233.5 eV correspond to the $3d_{5/2}$ and $3d_{3/2}$ orbitals of Mo^{4+} in MoO_2 [18], whereas those at 232.6 and 235.8 eV are attributable to Mo^{6+} in MoO_3 , likely arising from surface oxidation of the molybdenum species in the

$N@Mo_2C/V_2O_3$ [8, 18, 50, 51]. Notably, compared to $N@Mo_2C$, the Mo^{3+} and Mo^{4+} peaks in $N@Mo_2C/V_2O_3$ exhibit reduced intensity, whereas the Mo^{6+} peak becomes more pronounced and shows a slight positive shift (~ 0.15 eV) in binding energy. This observation suggests that the incorporation of V_2O_3 induces interfacial charge redistribution in $N@Mo_2C/V_2O_3$, leading to electron depletion from Mo and a consequent increase in its oxidation state. Charge transfer at the heterojunction interface is also expected to influence the valence states of neighboring V species. As illustrated in Fig. 2(c), the V 2p spectrum reveals that the binding energies of V^{3+} (515.22 and 522.74 eV), V^{4+} (516.50 and 524.11 eV), and V^{5+} (517.53 and 525.22 eV) in $N@Mo_2C/V_2O_3$ are slightly lower (~ 0.1 eV) than those in pristine V_2O_3 [26, 52, 53]. This shift implies strong interfacial charge transfer between the two components in the $N@Mo_2C/V_2O_3$ cluster heterostructure, which may enhance the activation of catalytic sites.

Additionally, the C 1s spectrum (Fig. 2(d)) exhibits multiple fitted peaks, where the minor shoulder at 283.26 eV corresponds to the C–Mo bond in Mo_2C [15]. The dominant peak at 284.8 eV is assigned to graphitic carbon (C–C), whereas the signal at 286.31 eV arises from nitrogen-doped carbon (C–N) [54, 55]. A weak peak at 288.23 eV is attributable to C–O bonding. Figure 2(e) shows the high-resolution N 1s spectrum, confirming the presence of Mo 3p (395.03 eV), Mo–N (397.50 eV), pyridinic-N (398.82 eV), pyrrolic-N (400.40 eV), and graphitic-N (401.40 eV) [50, 51]. The detection of Mo–N bonds in $N@Mo_2C/V_2O_3$ confirms the successful incorporation of nitrogen into the Mo_2C lattice. Moreover, previous studies indicate that pyrrolic nitrogen acts as an active site for the HER and effectively improves the electrical conductivity of the carbon substrate [56]. In the O 1s spectrum (Fig. 2(f)), the fitted peaks at 533.10, 532.03, and 530.73 eV are assigned to adsorbed water molecules, O–C, and O–Mo bonds [50], respectively.

3.3 Electrochemical performance

The electrocatalytic HER performance of the $N@Mo_2C/V_2O_3$ cluster heterostructure was evaluated using a standard three-electrode system in 1.0 M KOH alkaline electrolyte. To optimize the activity of cluster heterostructure catalysts, the effects of precursor loading and pyrolysis temperature on their phase composition and HER performance were systematically examined (Figs. S6 and S7 in the ESM). Optimal HER performance was achieved with a precursor loading of 10 μmol and a pyrolysis temperature of 650 °C, conditions under which well-defined coexisting Mo_2C and V_2O_3 phases were formed. For comparative analysis, control samples of $N@Mo_2C$ and V_2O_3 were synthesized and tested under identical conditions.

XRD analysis (Fig. S8 in the ESM) reveals that the incorporation of V_2O_3 in the $N@Mo_2C/V_2O_3$ cluster heterostructure effectively suppresses particle agglomeration compared to single-phase $N@Mo_2C$ derived from Mo_6-6NAr , leading to enhanced HER activity. To ensure rigorous performance benchmarking, commercially available 20 wt.% Pt/C was used as a reference catalyst. As shown in Fig. 3(a), the Pt/C catalyst exhibits a low overpotential of 20 mV to achieve a current density (j) of $10 \text{ mA}\cdot\text{cm}^{-2}$, whereas the $N@Mo_2C/V_2O_3$ cluster heterostructure requires a higher overpotential of ~ 67 mV. However, at overpotentials (η) exceeding 160 mV, the cathodic current of the $N@Mo_2C/V_2O_3$ cluster heterostructure increases sharply, eventually surpassing that of the Pt/C catalyst. This enhanced performance suggests that the integrated heterojunction catalyst, directly grown

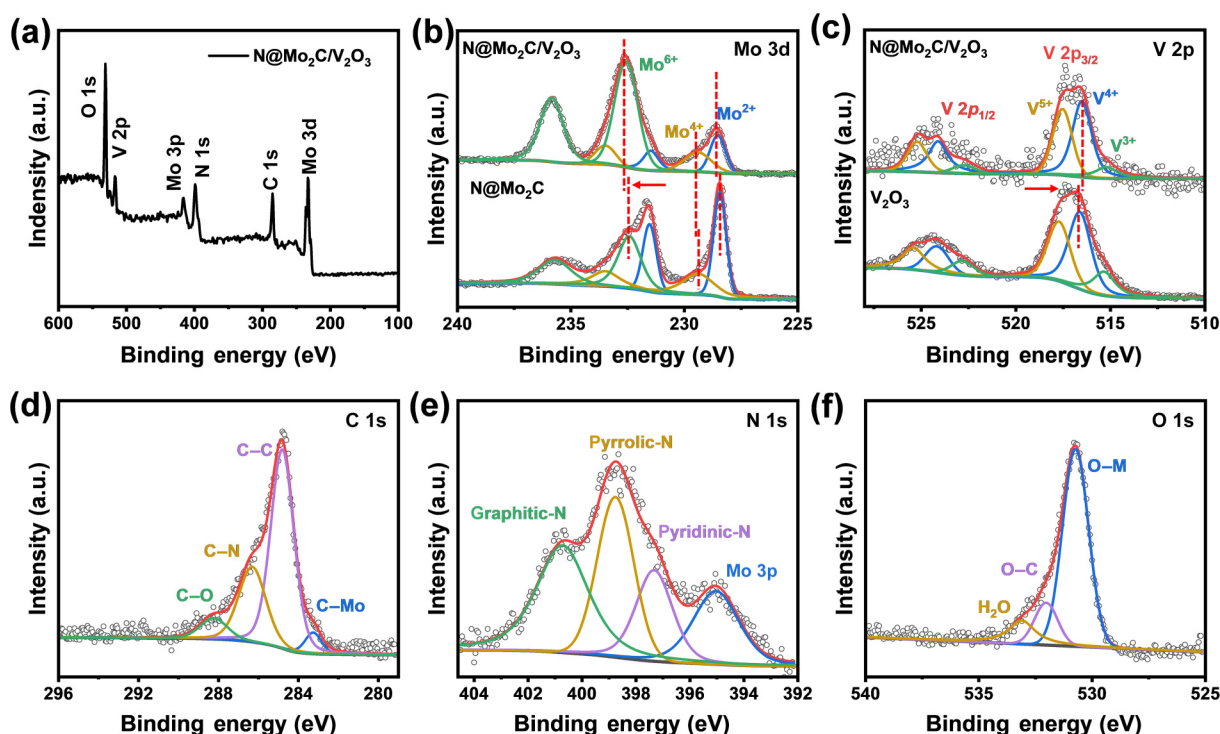


Figure 2 XPS analysis of N@Mo₂C/V₂O₃. (a) XPS survey spectrum of N@Mo₂C/V₂O₃. (b)–(f) High-resolution XPS signals of (b) Mo 3d; (c) V 2p; (d) C 1s; (e) N 1s; (f) O 1s.

on carbon paper, facilitates superior reaction kinetics by promoting efficient mass and charge transfer during the electrochemical process. Furthermore, the Tafel slope of N@Mo₂C/V₂O₃ at low current density was determined to be 64 mV·dec⁻¹ (Fig. 3(b)), higher than that of commercial Pt/C (38 mV·dec⁻¹) but significantly lower than those of pristine N@Mo₂C and V₂O₃ (75 and 317 mV·dec⁻¹, respectively). This indicates that the HER on the N@Mo₂C/V₂O₃ cluster heterostructure proceeds via the Volmer–Heyrovsky mechanism. Notably, N@Mo₂C/V₂O₃ achieves an impressive current density of 300 mA·cm⁻² at a low overpotential of just 191 mV (Fig. 3(c)), outperforming commercial Pt/C (239 mV) and most previously reported non-noble metal catalysts. Combined with its cost-effectiveness and high efficiency, the N@Mo₂C/V₂O₃ cluster heterostructure exhibits exceptional HER performance under high-current conditions, demonstrating its significant potential for commercial electrolyzer applications.

The C_{dl} , determined through CV measurements in the non-Faraday potential region at various scan rates (Fig. S9 in the ESM), serves as a reliable indicator of the electrochemically active surface area (ECSA) [57]. As shown in Fig. 3(d), the N@Mo₂C/V₂O₃ cluster heterostructure exhibits a remarkably high C_{dl} of 137 mF·cm⁻², substantially surpassing those of its individual components (120 mF·cm⁻² for N@Mo₂C and 52 mF·cm⁻² for V₂O₃). These results clearly demonstrate that the dual-component N@Mo₂C/V₂O₃ cluster heterostructure provides abundant active sites, which directly correlates with its superior HER performance. EIS is commonly employed to investigate charge transfer kinetics in electrocatalytic systems [34, 58]. As shown in Fig. S10 and Table S3 in the ESM, the N@Mo₂C/V₂O₃ cluster heterostructure exhibits a significantly lower charge transfer resistance (1.99 Ω) compared to its individual components (N@Mo₂C and V₂O₃), reflecting its superior charge transfer efficiency and enhanced HER kinetics [59]. Further EIS measurements were performed on N@Mo₂C/V₂O₃ at

different applied potentials, as illustrated in the Nyquist and Bode plots (Figs. S10(c) and S10(d) in the ESM). The impedance spectra reveal consistent electrochemical behavior across various overpotentials, indicating stable reaction kinetics throughout the HER process. In addition, the charge transfer resistance decreases progressively with increasing potential, confirming that the N@Mo₂C/V₂O₃ cluster heterostructure can maintain excellent HER performance even under high-current density conditions [34].

The electrochemical stability of the N@Mo₂C/V₂O₃ cluster heterostructure was evaluated over 3,000 consecutive CV cycles. As illustrated in Fig. 3(e), the polarization curves before and after cycling are nearly identical, with no observable potential shift. Furthermore, post-stability characterization confirmed that the phase structure and chemical composition of the N@Mo₂C/V₂O₃ cluster heterostructure remained unchanged compared to the pristine catalyst (Fig. S11 in the ESM), demonstrating outstanding electrochemical and structural stability under alkaline conditions. The long-term stability of the N@Mo₂C/V₂O₃ electrode under high-current density conditions was further evaluated through chronoamperometry (Fig. 3(f)). Remarkably, the catalyst maintained exceptional stable operation at 110 mA·cm⁻² with negligible current density decay over 400 h of continuous operation. These results confirm the outstanding durability of N@Mo₂C/V₂O₃ under high-current conditions in alkaline media, which is crucial for practical applications. Comparative analysis with previously reported alkaline-stable molybdenum-based HER catalysts (Fig. 3(g) and Table S4 in the ESM) reveals that N@Mo₂C/V₂O₃ exhibits superior performance, positioning it as a leading candidate within this material class with significant potential for commercial implementation.

To assess the HER selectivity of the N@Mo₂C/V₂O₃ cluster heterostructure, its Faradaic efficiency was measured (Fig. 4(a)). The calculated Faradaic efficiency approaches 100%, confirming

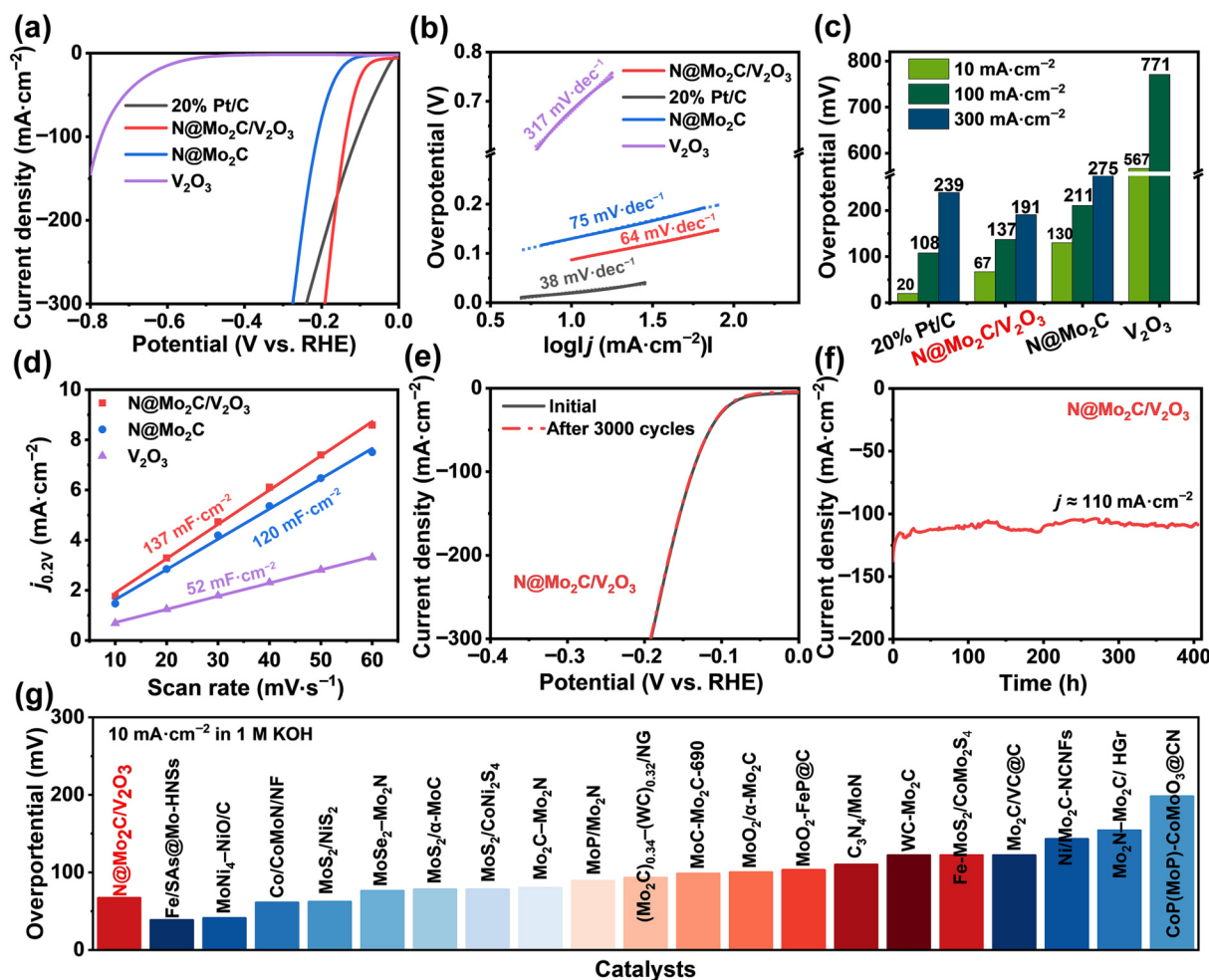


Figure 3 Electrocatalytic activity of the as-prepared materials for the HER in alkaline medium (1.0 M KOH). (a) *iR*-corrected polarization curves and (b) corresponding Tafel plots of the materials: N@Mo₂C/V₂O₃, N@Mo₂C, V₂O₃, and commercial 20 wt.% Pt/C. (c) Overpotentials at 10, 100, and 300 mA·cm⁻². (d) The *C*_{dl} of different catalysts. (e) LSV curves of the N@Mo₂C/V₂O₃ recorded before and after 1000 CV cycles of the HER. (f) Chronoamperometric curve of the N@Mo₂C/V₂O₃ at a constant potential of -0.14 V vs. RHE for 400 h. (g) Comparison of HER performances in 1.0 M KOH for N@Mo₂C/V₂O₃ with other reported catalysts.

near-perfect electrochemical selectivity for the HER. Additionally, a solar-driven water electrolysis device was constructed, directly powered by solar panels, as shown in Fig. 4(b) and Fig. S12 in the ESM. Even under continuous fluctuations in solar irradiance, N@Mo₂C/V₂O₃ remains stable in performing HER through water electrolysis (Fig. 4(c) and Table S5 in the ESM). The system achieved a hydrogen production rate of ~ 43 mL within 10 min, highlighting its potential for renewable energy applications. Based on the measured 100% Faraday efficiency, this corresponds to an effective current density of ~ 617 mA·cm⁻² utilized by the catalytic electrode for hydrogen production. These findings demonstrate that the N@Mo₂C/V₂O₃ cluster heterostructure is a promising candidate for renewable hydrogen production in photoelectrochemical water-splitting systems.

To evaluate the commercial potential of N@Mo₂C/V₂O₃ cluster heterostructure for water electrolysis, large-area, self-supported N@Mo₂C/V₂O₃ electrodes were fabricated and employed as cathodes in AWE cells. Cell performance was evaluated with commercial Raney nickel or literature-reported NiFe-LDH catalysts serving as the anode. All electrochemical measurements were performed in a 30% KOH electrolyte at 60 °C under atmospheric pressure, without *iR* compensation. As shown in Fig. S13 in the ESM, when coupled with a commercial Raney nickel anode, the

N@Mo₂C/V₂O₃ cathode achieved a current density of 500 mA·cm⁻² at an applied voltage of 2.0 V. Although slightly less efficient than Pt/C at lower current densities (< 200 mA·cm⁻²), the N@Mo₂C/V₂O₃||Zirfon||Raney nickel system exhibited a distinct advantage at higher current densities (> 200 mA·cm⁻²), requiring a significantly lower operating voltage. The replacement of the conventional anode with a NiFe-LDH anode (Fig. 4(d)) notably improved overall performance of the N@Mo₂C/V₂O₃||Zirfon||NiFe-LDH electrolysis cell. Specifically, the cell voltage required to achieve 500 and 1000 mA·cm⁻² decreased to 1.94 and 2.35 V, respectively, markedly lower than the 2.04 and 2.54 V needed for a Pt/C-based cell to reach the same high current densities. Under alkaline electrolyzer conditions, our catalyst exhibits moderate performance compared with previously reported catalysts (Table S6 in the ESM). Figure 4(f) shows the disassembled electrolysis cell, showing the sequence of components: anode shell, anode plate, anode current collector, anode catalyst, flow channel and reaction chamber (with commercial Zirfon separator), cathode catalyst, cathode current collector, cathode plate, and cathode shell. To ensure accuracy in evaluation, all assembly tests were repeated thrice, and the results were averaged. Furthermore, the performance of the AWE was further investigated at varying temperatures, demonstrating a positive correlation between

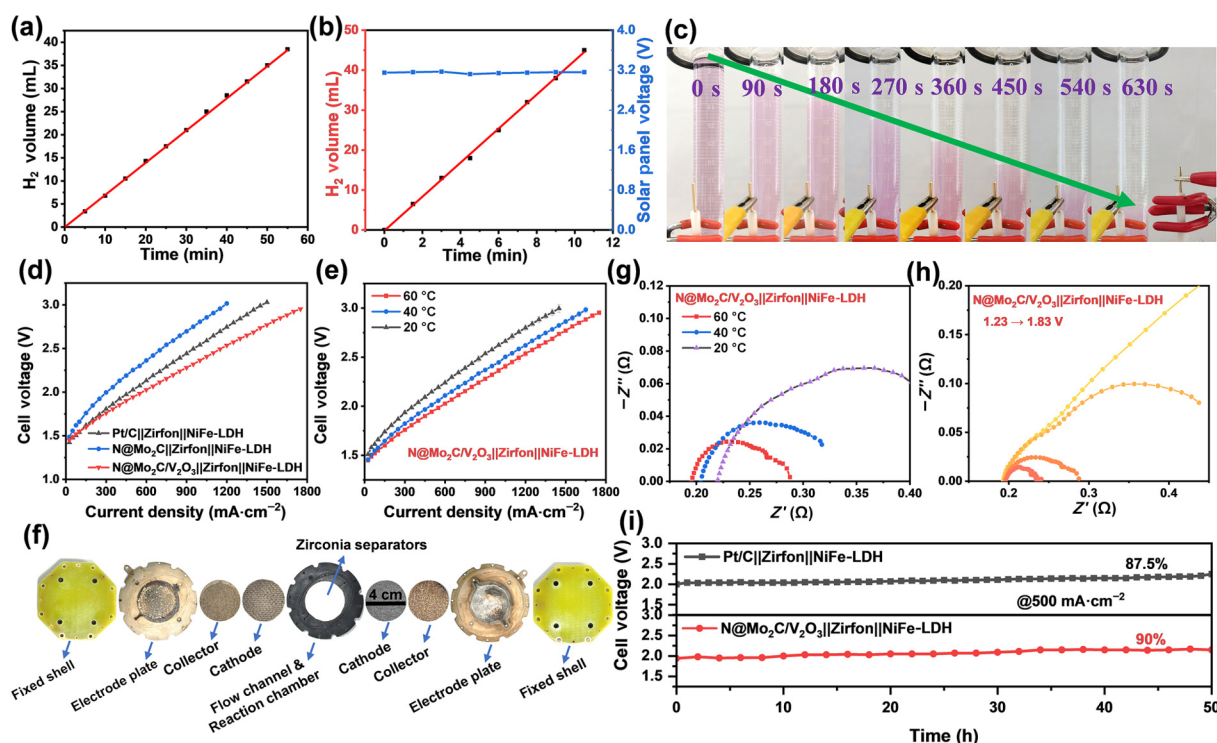


Figure 4 (a) Faraday efficiency test of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ at $100 \text{ mA}\cdot\text{cm}^{-2}$, the dots in the figure represent tested data and the red line represents the theoretical value. (b) Solar panel coupled electrolysis of water for hydrogen production test. (c) Schematic of hydrogen collection by drainage method. (d) Performance of $\text{Pt/C}||\text{Zirfon}||\text{NiFe-LDH}$, $\text{N@Mo}_2\text{C/C}||\text{Zirfon}||\text{NiFe-LDH}$, and $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3||\text{Zirfon}||\text{NiFe-LDH}$ electrolytic cell. (e) Performance of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3||\text{Zirfon}||\text{NiFe-LDH}$ electrolytic cell at different temperatures. (f) The sequence of components after disassembling the electrolysis cell. (g) EIS of the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3||\text{Zirfon}||\text{NiFe-LDH}$ electrolytic cell (g) at various temperatures and (h) under different voltages (1.23, 1.43, 1.63, and 1.83 V). (i) Curves of cell voltage variation with respect to time of $\text{Pt/C}||\text{Zirfon}||\text{NiFe-LDH}$ and $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3||\text{Zirfon}||\text{NiFe-LDH}$ at $500 \text{ mA}\cdot\text{cm}^{-2}$ and 60°C in 30 wt. % KOH.

operating temperature and electrolyzer efficiency (Fig. 4(e)).

To elucidate the origin of the performance enhancement, EIS measurements were performed on the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3||\text{Zirfon}||\text{NiFe-LDH}$ electrolytic cell at various temperatures (Fig. 4(g)). The results revealed optimal charge transfer kinetics and reaction rates at 60°C . Additional EIS measurements at different potentials showed consistent electrochemical kinetics throughout the water-splitting process, with further improvements in charge transfer kinetics at elevated potentials (Fig. 4(h)). This study also found that, compared to a conventional three-electrode system, the compact architecture of the electrolysis cell reduces ohmic resistance, enhancing electrolysis performance and efficiency. Finally, the long-term stability of the AWE was evaluated at an industrial current density of $500 \text{ mA}\cdot\text{cm}^{-2}$ (Fig. 4(i)). The $\text{Pt/C}||\text{Zirfon}||\text{NiFe-LDH}$ configuration demonstrated moderate stability, with the cell potential rising to 2.25 V after 50 h of continuous operation, corresponding to 87.5% retention of the initial performance. By contrast, the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ -based electrolyzer showed superior stability, maintaining 90% of its initial performance under identical conditions. The enhanced stability of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ can be attributed to its integrated, self-supported electrode architecture, which eliminates the need for polymeric binders that typically obstruct active sites and impede mass and electron transfer. Furthermore, the *in situ* growth of the catalyst on a conductive substrate provides robust interfacial adhesion, effectively mitigating material detachment during prolonged operation. These combined structural advantages underscore the strong potential of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ for industrial-scale hydrogen production [5].

3.4 Interpretation of the structure–activity relationship

A proportional mixture of Mo6-NAr and V10 was prepared to explore the advantages of dual-component heterojunctions. The mixture was subsequently grown and loaded onto CFP and then pyrolyzed in a H_2/Ar atmosphere at 650°C for 3 h. As shown in the XRD pattern (Fig. S14(a) in the ESM), the resulting product consists of two distinct phases, $\text{N@Mo}_2\text{C}$ and V_2O_3 , denoted as $\text{N@Mo}_2\text{C}+\text{V}_2\text{O}_3$, which can also be obtained through simple physical mixing and pyrolysis. However, the XRD diffraction peaks of the physically mixed sample are more intense compared to the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure, suggesting a larger grain size for the $\text{N@Mo}_2\text{C}$ nanoparticles. This is likely attributed to the severe aggregation of nanoparticles during sintering. The HER performance evaluation of the two catalysts demonstrated that the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure, synthesized from the well-designed $\text{Mo}_3\text{V}_4\text{-6NAr}$ precursor, exhibited significantly enhanced catalytic activity than the physically mixed $\text{N@Mo}_2\text{C}+\text{V}_2\text{O}_3$ (Fig. S14(b) in the ESM). This superior performance can be attributed to the abundant heterointerfaces in $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$, which provide numerous active sites, highlighting the critical role of precursor molecular design in optimizing catalytic properties. Furthermore, the physically mixed samples displayed inferior electrochemical stability, with notable performance degradation after 3,000 CV cycles (Fig. S15(a) in the ESM). XRD patterns (Fig. S15(b) in the ESM) revealed a significant decrease in peak intensity corresponding to $\text{N@Mo}_2\text{C}$ in the $\text{N@Mo}_2\text{C}+\text{V}_2\text{O}_3$ composite after the HER test, suggesting potential structural degradation during the catalytic process. SEM characterization (Fig. S16 in the ESM)

further confirmed that the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ nanosheets underwent size reduction and exfoliation following the HER, confirming the poor mechanical stability of catalysts prepared via simple physical mixing.

Furthermore, we conducted a comprehensive analysis of the hydrophilicity, dynamic behavior of hydrogen bubble growth and desorption on the electrode surface, and electrical conductivity of the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure to investigate its outstanding performance at high current densities. Under alkaline conditions, superior hydrophilicity facilitates the adsorption of water molecules on catalytic surfaces, thereby promoting water dissociation. Water contact angle measurements (Fig. 5(a) and Fig. S17 in the ESM) demonstrated that pristine CFP (127.1°) is hydrophobic, whereas $\text{N@Mo}_2\text{C}$ (97.4°) shows only moderate hydrophilicity. By contrast, both V_2O_3 (19.7°) and $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ (18.9°) display significantly enhanced hydrophilicity, confirming that the introduction of V_2O_3 substantially enhances interfacial hydrophilicity. During hydrogen evolution, the size and detachment behavior of hydrogen bubbles provide macroscopic

insight into the gas–liquid–solid interfacial properties of the catalyst surface. As shown in Fig. 5(b) and Movie S1 in the ESM, at a current density of $200 \text{ mA}\cdot\text{cm}^{-2}$, hydrogen bubbles formed on V_2O_3 and $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ are noticeably smaller and detach more readily than those observed on Pt/C and $\text{N@Mo}_2\text{C}$. This behavior suggests that $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ exhibits more faster bubble detachment and more efficient gas release compared to pristine V_2O_3 and $\text{N@Mo}_2\text{C}$, thereby helping to maintain the exposure of active sites during prolonged hydrogen evolution. Resistivity measurements (Fig. 5(c) and Fig. S18 in the ESM) further revealed that V_2O_3 , $\text{N@Mo}_2\text{C}$, and $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ exhibit resistivities of 1, 0.02575, and $0.0407 \Omega\cdot\text{cm}$, respectively, confirming that the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ heterojunction retains the high intrinsic electrical conductivity of $\text{N@Mo}_2\text{C}$. Collectively, these findings demonstrate that in the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure, $\text{N@Mo}_2\text{C}$ serves as the primary active site with superior charge transfer capability, while V_2O_3 synergistically enhances hydrophilicity and hydrogen desorption kinetics. This dual functionality underpins the exceptional HER performance of the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure at high current densities.

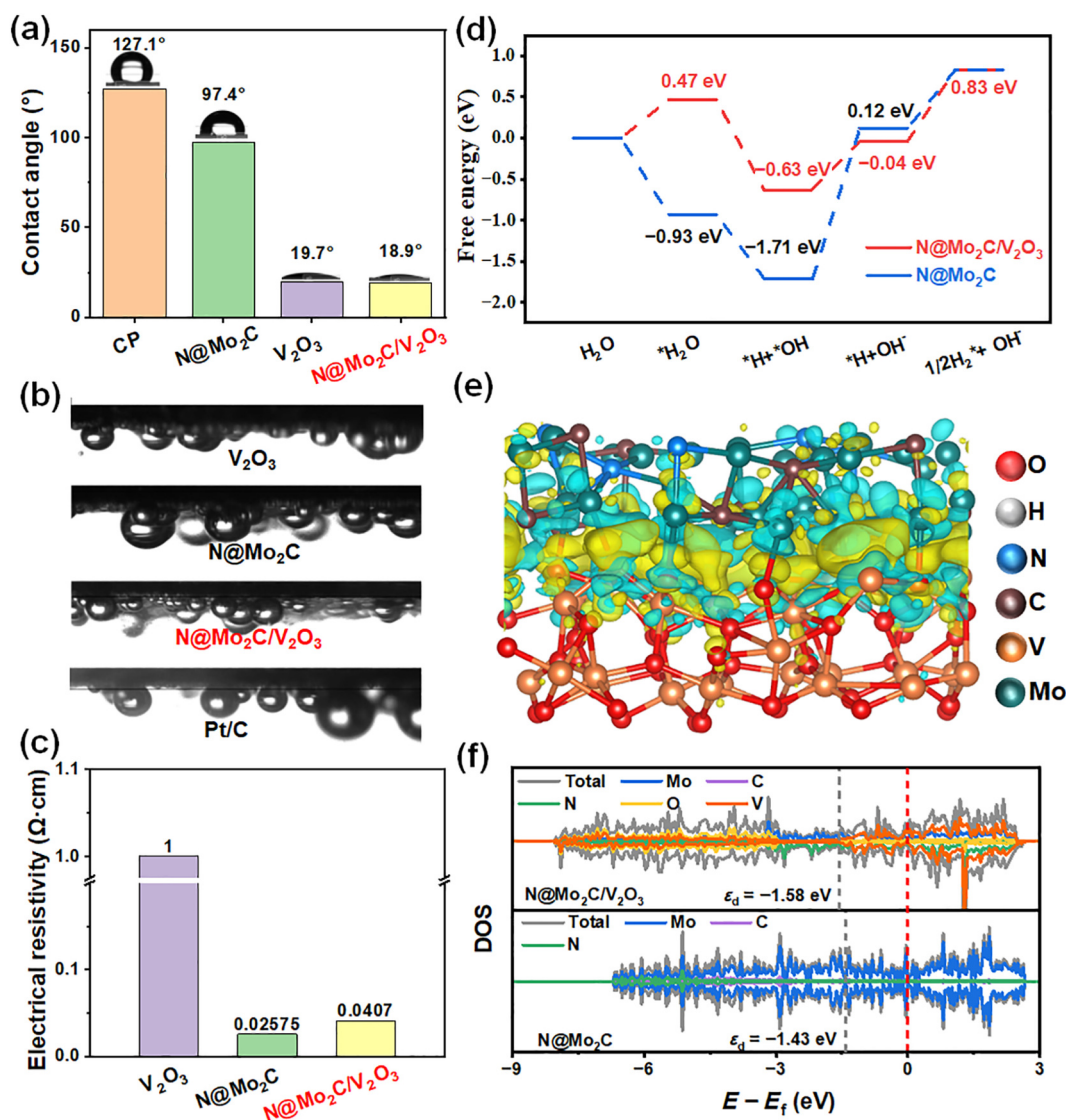


Figure 5 (a) Water contact angle. (b) *In situ* electron micrographs of the desorption of hydrogen. (c) Electrical resistivity of $\text{N@Mo}_2\text{C}$, V_2O_3 , and $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$. (d) Reaction energy profiles of the complete alkaline HER reaction on the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ and $\text{N@Mo}_2\text{C}$ system models. (e) Differential charge density diagram of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$. (f) DOS spectra of Mo 4d for $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ and $\text{N@Mo}_2\text{C}$.

To elucidate the mechanism underlying the enhanced alkaline HER activity, density functional theory (DFT) calculations were conducted on the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure. The structural model was constructed based on XRD and HRTEM results, featuring an interfacial configuration where $\text{N@Mo}_2\text{C}(121)$ interfaces with $\text{V}_2\text{O}_3(110)$ planes to form a crystalline heterojunction, as shown in Fig. S19 in the ESM. In alkaline media, the HER proceeds through sequential water adsorption, H_2O dissociation (Volmer step), OH^- desorption, and H_2 formation/desorption (Heyrovsky step) [60]. Our experimental results confirm that the overall reaction follows the Volmer–Heyrovsky pathway. A comparative investigation of the reaction pathways on $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ and its single-component counterpart, $\text{N@Mo}_2\text{C}$, is shown in Figs. S20 and S21 in the ESM. As illustrated in Fig. 5(d), $\text{N@Mo}_2\text{C}$ exhibits a relatively low water adsorption energy of -0.93 eV. However, the OH^- desorption step constitutes the rate-limiting step for $\text{N@Mo}_2\text{C}$, with a considerable energy barrier of 1.83 eV that severely restricts HER kinetics [8]. By contrast, while the water adsorption energy for the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure is slightly higher (0.43 eV), the interfacial interaction significantly facilitates the water dissociation and reduces the OH^- desorption energy barrier to 0.59 eV, which is much lower than that of $\text{N@Mo}_2\text{C}$. This considerable reduction in the OH^- desorption barrier greatly improves the overall reaction rate. Moreover, the energy barrier of the rate-determining step for $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ is 0.87 eV, much lower than that of $\text{N@Mo}_2\text{C}$ (1.83 eV), indicating that the optimized $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure can effectively promote HER kinetics and leads to superior catalytic performance in alkaline media. The overall smoothness of the reaction pathway, with no kinetically prohibitive steps, ensures efficient reaction progress with minimal resistance, thus contributing to the excellent HER activity of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$.

To further explore the impact of the electronic structure on the enhanced alkaline HER activity of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$, differential charge density and density of states (DOS) analyses were performed [61, 62]. The charge density difference analysis (Fig. 5(e)) reveals distinct regions of electron accumulation (yellow) and depletion (cyan), demonstrating an inhomogeneous charge distribution at the $\text{N@Mo}_2\text{C}-\text{V}_2\text{O}_3$ interface. Notably, significant electron transfer occurs from $\text{N@Mo}_2\text{C}$ to interfacial V_2O_3 , creating a polarized charge distribution within the V–O–Mo interfacial system. Further, DOS analysis reveals continuous states at the Fermi level for both $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ and $\text{N@Mo}_2\text{C}$ (Fig. 5(f)), confirming their metallic character and high electronic conductivity [33]. The d-band center (ϵ_d) calculations demonstrate that Mo sites in $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ exhibit a lower ϵ_d value (-1.58 eV) compared to pristine $\text{N@Mo}_2\text{C}$ (-1.43 eV), representing a 0.15 eV downward shift relative to the Fermi level. This negative ϵ_d shift correlates with weakened hydrogen adsorption energy, which simultaneously promotes H_2 desorption and enhances the HER kinetics of $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ [60, 62]. Consequently, the superior HER activity of the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ heterojunction arises from three key synergistic effects: (i) thermodynamically favorable OH^- desorption, which substantially lowers the energy barrier of the rate-determining step; (ii) moderated hydrogen adsorption free energy, which facilitates hydrogen release at the catalyst surface and is consistent with the experimentally observed formation of small, readily detachable hydrogen bubbles; (iii) enhanced electronic conductivity originating from the polarized V–O–Mo interfacial structure. Collectively, these factors enable efficient interfacial charge transport and

smooth reaction pathways, thereby endowing $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ with excellent catalytic performance in alkaline media.

4 Conclusion

Herein, we successfully synthesized a POM molecule precursor ($\text{Mo}_3\text{V}_4\text{-6NAr}$) with well-defined Mo–O–V and Mo–N bonds and subsequently constructed ultrafine $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructures via high-temperature pyrolysis. The superior HER performance of the optimized $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructure originates from electronically tuned interfacial structures, including interfacial charge redistribution (as evidenced by the positive shift of Mo 3d and the negative shift of V 2p in XPS) and the downshift of the Mo d-band center ($\Delta\epsilon_d \approx -0.15$ eV) revealed by DFT calculations. These electronic modifications optimize hydrogen adsorption strength of Mo active sites, accelerate electron transfer across the interface of the $\text{N@Mo}_2\text{C}/\text{V}_2\text{O}_3$ cluster heterostructures, and enhance overall HER kinetics. As a result, the optimized catalyst achieves a current density of $300 \text{ mA}\cdot\text{cm}^{-2}$ at an overpotential of 191 mV and maintains stable operation for more than 400 h . In an AWE, it delivers $500 \text{ mA}\cdot\text{cm}^{-2}$ at 1.94 V , outperforming commercial $20 \text{ wt.}\%$ Pt/C. This study provides new insights into the rational design of high-performance, cost-effective cluster heterostructure catalysts and elucidates the synergistic roles of catalytic and co-catalytic active sites in regulating interfacial electron transfer and reaction pathways at the atomic level. Future research will focus on *in situ* spectroscopic monitoring of interfacial electronic states and precise modulation of coordination environments to further refine d-band tuning and hydrogen adsorption thermodynamics.

Electronic Supplementary Material: Supplementary material (including the preparation methods of the catalysts, the FT-IR, SEM, TEM, BET, Raman and XRD of the prepared samples, the TGA, XPS, ICP, the electrochemical data, and the structural model of the catalysts) is available in the online version of this article at <https://doi.org/10.26599/POM.2026.9140110>.

Data availability

All data needed to support the conclusions in the paper are presented in the manuscript and the Electronic Supplementary Material. Additional data related to this paper may be requested from the corresponding author upon request.

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Declaration of competing interest

The authors have no competing interests to declare that are relevant to the content of this article.

Author contribution statement

L. L. C: Data curation, visualization, writing manuscript. Y. C. H: Conceptualization, supervision, project administration, funding acquisition. H. T. L: Experimental design, visualization, methodology. R. L. G: Visualization, supervision. H. T: Investigation. J. W. C: Validation. Y. F. W: Investigation. M. H. L: funding acquisition, supervision. C. D. W: Supervision, resources. All the authors have approved the final manuscript.

Use of AI statement

None.

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